EXPERIMENTAL INVESTIGATION OF STATIC SETTLED CONCENTRATION OF MULTI-SIZED COKING COAL-WATER SLURRY

Salman Beg¹ and Deo Raj Kaushal²

¹Civil Engineering Department, Indian Institute of Technology, Delhi, New Delhi, India, Email: salmanbeg1988@gmail.com; ²Civil Engineering Department, Indian Institute of Technology, Delhi, New Delhi, India, Email: kaushal@civil.iitd.ac.in

In this experimental study, the effect of variation of coking coal concentration (C_w) and particle size proportions on static settled concentration by weight (C_{wss}) of multi-sized coking coal-water slurry is investigated using a graduated cylindrical flask. It is observed that, at 72 hours, the multi-sized coking coal-water slurry achieved maximum static settled concentration for each slurry concentration. From 0 hours to 24 hours, static settled concentration increases and then decreases from 24 hrs to 72 hours in each case of coking coal concentration and particle size proportion. For first particle size combination $C_1 = [(4 \text{ mm to } 3.15 \text{ mm}) + (3.15 \text{ mm to } 0.5 \text{ mm})]$, maximum C_{wss} at 72 hours decreases from Cw = 50% to 55% and then increases from 55% to 65% for both sets of particle size proportions P_{C11} and P_{C12} . For second particle size combination $C_2 = [(6.7 \text{ mm to } 3.15 \text{ mm}) + (3.15 \text{ mm to } 0.5 \text{ mm})]$, maximum C_{wss} at 72 hours increases from $C_w = 50\%$ to 55% and then increases from $C_2 = [(6.7 \text{ mm to } 3.15 \text{ mm to } 0.5 \text{ mm}) + (less than 0.5 \text{ mm})]$, maximum C_{wss} at 72 hours increases from $C_w = 50\%$ to 55% of to 65% for particle size proportions P_{C11} and P_{C12} . For second particle size combination $C_2 = [(6.7 \text{ mm to } 3.15 \text{ mm to } 0.5 \text{ mm}) + (less than 0.5 \text{ mm})]$, maximum C_{wss} at 72 hours increases from $C_w = 50\%$ to 65% for particle size proportions P_{C21} and for P_{C22} , maximum C_{wss} decreases from $C_w = 50\%$ to 55% and then increases from 55% to 65%. Out of the the selected concentrations of coking coal, the optimum value of Cw is observed as 55% for each set of particle size proportions P_{C11} , P_{C12} , P_{C21} , and P_{C22} corresponding in both particle size combinations C_1 and C_2 .

KEYWORDS: Coking Coal, Slurry, Static settled concentration, Particle Size Proportion.

NOTATION

C_w	Concentration of coking coal sample (%)
Cwss	Static settled concentration by weight (%)
C ₁	First particle size combination
C_2	Second particle size combination
m _s	Mass of solid particles in settled part of slurry (g)
P _{C11} and P _{C12}	Sets of particle size proportions corresponding to C ₁
P _{C21} , and P _{C22}	Sets of particle size proportions corresponding to C ₂
PSD	Particle size distribution
V _{lm}	Volume of water in settling slurry = $V_1 - (V_{mi} - V_m)$ (ml)
V _{mi}	Initial volume of slurry (ml)
Vm	Volume of settled slurry at any given time (ml)
V_1	Volume of water taken (ml)
Ws	Total required weight of coking coal sample (g)

ISSN 0867-7964 ISBN 978-83-7717-323-7 DOI 10.30825/4.12-41.2019

 W_{w} ρ_{l} Weight of 500 ml water taken in measuring cylinder (g) Density of water (g/cm^3)

1. INTRODUCTION

Coal plays an essential role in the development of a country as it is one of the significant sources of energy. Coal available in its natural form is used for power generation while coking coal is used in metallurgical and steelmaking industries. Hence, it is transported to the vicinity of use in its natural form or as a refined product (National Academy of Engineering 1974). Transport of coking coal to the point of use in the form of slurry through pipelines and launders is one of the efficient means which is growing day by day (National Academy of Engineering 1974). For transporting the coal-water slurry, pipelines are used for long distances while open channel flumes/launders are used in the mining industries to transport slurries during processing and to disposal sites (Burger 2014).

For transporting the coal as slurry through pipeline and flumes, the coal is mixed with water and pumped through a pipe or channelized through the open channel flumes to the point of use where the coal is removed from the water by means of centrifuges, vacuum filters, or thermal drying (National Academy of Engineering 1974). Two-phase system of slurry and properties associated with coal (specific gravity, moisture content, ash content, hardness, size and shape of coal particles, surface texture and particle size distribution) makes its pumping more complex (Sheshadri et al. 1997; Kaushal et al. 2002). The concentration of coal in water, temperature and viscosity are the properties of coal water slurry (National Academy of Engineering 1974).

As water plays a significant role in the preparation of slurries, its usage and availability are critical in countries where there are strict water usage management programs. Therefore a particular slurry transportation system (pipeline or open channel flume) becomes unfeasible if its water requirement is very high. The optimization of pipeline and flume design involves the maximization of solids transport efficiency while at the same time, reduces water usage (Burger 2014). To utilize a lower amount of water for transporting the maximum amount of coal through pipelines and open channel flumes/launders, the concentration of coal has to be increased beyond 50% by weight (Faddick 1979). When there is a power cut for long durations than possibilities of pipeline choking increases due to the settlement of coarser coal particles at the bottom of the pipe which increases the chances of pipeline burst due to abrasion of pipe material (National Academy of Engineering 1974). Mixing of powdered particles along with coarser particles will help in reducing the viscosity and provide ease in the movement of slurry at lower velocities (National Academy of Engineering 1974).

Nguyen et al. (1997) experimentally investigated the effect of variation of particle sizes on rheological behaviour of unimodal, bimodal and trimodal coal-water slurry. They concluded that at any given concentration of solid, the slurry viscosity can significantly be reduced by mixing two or more different size fractions of solid and by controlling the amount of the different size fractions. An experimental study conducted by Mishra (1996) for the flow of multi-sized slurry in horizontal pipelines reveals that static settled concentration increases with increase in particle size and decreases with an increase in particle density. Gandhi and Borse (2002) used sand-water slurry to analyze the effect of particle size distribution on the wear of cast iron pipe. They observed a linear increase in wear with an increase in particle size. On the basis of specific energy consumption, optimum concentration of solid is generally 5-10% lower than the maximum static settled concentration (Biswas et al. 2000; Singh et al. 2017).

Number of studies has been conducted on the effect of particle size distribution on the rheology of the coal-water slurry (Leong et al. 1987; Round and Hessari 1987; Toda and Kuriyami 1988; Sengun and Probstein 1989; Turian et al. 1992; Roh et al. 1995; Singh et al. 2016). No study has been carried out to find the maximum settled concentration value at higher concentrations of multi-sized coking coal-water slurry for its transportation through the pipeline and launder.

In this paper, an effort has been made to experimentally investigate the behavior of maximum static settled concentration under the variation of particle size proportion and concentration for highly concentrated multi-sized coking coal-water slurry.

2. MATERIALS AND METHODOLOGY

The sieve analysis method was used to obtain the PSD of coking coal particles larger than 75 μ m and for the PSD of coking coal particles smaller than 75 μ m, hydrometer analysis technique was used. IS:460 standard sieves with sieve arrangement of 9.5 mm, 6.7 mm, 3.15 mm, 2.36mm, 1.18 mm, 710 μ m, 500 μ m, 300 μ m, 150 μ m and 75 μ m was used for sieve analysis. In sieve analysis, 1000 g of oven dried coking coal sample was sieved through sets of sieves and cumulative percent of solid retained on the sieves and cumulative percent of solid retained on the sieves and procedures. The standard 151H hydrometer was used for hydrometer analysis of particle sizes less than 75 μ m. The final PSD of coking coal was plotted on semi-log graph, which is presented in Figure 1.

For studying the effect of C_w and particle size proportions on C_{wss} of multi-sized coking coal-water slurry, the oven-dried coking coal was sieved by mechanical shaker through the first sieve arrangement of 4 mm, 3.15 mm, 0.5 mm and pan and second sieve arrangement of 6.7 mm, 3.15 mm, 0.5 mm and pan to obtain the required/selected particle size ranges 4 - 3.15 mm, 6.7 - 3.15 mm, 3.15 - 0.5 mm and less than 0.5 mm. To prepare the coking coal-water slurry having multi-sized distribution, two combinations (C_1 and C_2) of particle sizes was considered from the selected particle size ranges (table 1). For the variation of particle size proportion in the particle size combinations C_1 and C_2 , two sets of particle size proportions P_{C11} and P_{C12} were considered for particle size combination C_1 and two sets of P_{C21} and P_{C22} for particle size combination C_2 (Table 1).

500 ml tap water were taken in 1200 ml cylindrical measuring flask having a diameter of 50 mm and this amount of water in the flask was weighed. Now according to required slurry concentration ($C_w = 50\%$, 55%, 60% and 65% by weight), the amount of total coal required were calculated and the weight of the proportions of different particle size ranges in the total amount of required coking coal were also calculated. This weighted coking coal sample was then poured in measuring cylinder containing 500 ml tap water and the mixture was well shaken till it got mixed completely and uniformly. After thorough mixing, the cylinder was placed on the undisturbed surface. The reading of free water surface level and settled slurry level was recorded at 0, 24, 28, 48, 72 and 96 hrs. and then C_{wss} was calculated. These steps were repeated for $C_w = 50\%$ to 65% in both cases of C_1 and C_2 .

The equations used for calculating the required weight of coking coal sample (W_s) and static settled concentration by weight (C_{wss}) of coking coal are given below:

$$C_{w} = \frac{W_{s}}{W_{s} + W_{w}}$$
(1)

$$C_{w_{SS}} = \frac{m_s}{(\rho_l V_{lm} + m_s)} \tag{2}$$

Table 1

Selected particle size combinations and proportions of particle size ranges

C _w (%)	Particle size combination $C_1 = [(4 \text{ mm to } 3.15 \text{ mm}) + (3.15 \text{ mm to } 0.5 \text{ mm}) + (less than 0.5 \text{ mm})]$				
50, 55,	Proportions of particle size range in P_{C11}	$P_{4mm \text{ to } 3.15mm} = 10\%$	$P_{3.15mm to 0.5mm} = 45\%$	$\frac{P_{less than 0.5mm}}{45\%} =$	
60, 65	Proportions of particle size range in P _{C12}	$P_{4mm \text{ to } 3.15mm} = 15\%$	$\frac{P_{3.15mm \text{ to } 0.5mm}}{42.5\%} =$	$P_{less than 0.5mm} = 42.5\%$	
where $P_{C11} = [(P_{4mm to 3.15mm} = 10\%) + (P_{3.15mm to 0.5mm} = 45\%) + (P_{less than 0.5mm} = 45\%)]$ $P_{C12} = [(P_{4mm to 3.15mm} = 15\%) + (P_{3.15mm to 0.5mm} = 42.5\%) + (P_{less than 0.5mm} = 42.5\%)]$					
Cw(%)	Particle size combination $C_2 = [(6.7 \text{ mm to } 3.15 \text{ mm}) + (3.15 \text{ mm to } 0.5 \text{ mm}) + (less than 0.5 \text{ mm})]$				
50, 55, 60, 65	Proportions of particle size range in P_{C21}	$P_{6.7mm \text{ to } 3.15mm} = 10\%$	$P_{3.15mm to 0.5mm} = 45\%$	Pless than 0.5mm=45%	
	Proportions of particle size range in P _{C22}	$P_{6.7mm \text{ to } 3.15mm} = 15\%$	$P_{3.15mm \text{ to } 0.5mm} = 42.5\%$	$P_{\text{less than 0.5mm}} = 42.5\%$	
where, $P_{C21} = [(P_{6.7mm to 3.15mm} = 10\%) + (P_{3.15mm to 0.5mm} = 45\%) + (P_{less than 0.5mm} = 45\%)$ $P_{C22} = [(P_{6.7mm to 3.15mm} = 15\%) + (P_{3.15mm to 0.5mm} = 42.5\%) + (P_{less than 0.5mm} = 42.5\%)]$					

3. RESULTS AND DISCUSSION

From PSD, the maximum particle size of coking coal was recorded as 9500 μ m. The median diameter, d₅₀, of coking coal particle is 600 μ m (=0.6 mm) and d₉₀, d₈₅, d₂₅ and d₅ are 7000 μ m, 3700 μ m, 190 μ m and 59 μ m respectively. Only 8.423% particles are finer than 75 μ m, 89.53% particles are finer than 6700 μ m, nearly 86% particles are finer than 4000 μ m, 83.59% particles are finer than 3150 μ m and 45.42% particles are finer than 500 μ m. 2.41%, 5.9%, and 38.2% particles lie in the range of 4000-3150 μ m, 6700-3150 μ m and 3150-500 μ m respectively.



Figure 1. Particle size distribution of coking coal sample

From the experimental study, it is observed that the multi-sized coking coal-water slurry achieved maximum static settled concentration at 72 hours (readings were taken at 96 hour for surety) for each coking coal concentration (C_w) and particle size combinations C_1 and C_2 .

Table 2

Variation of C_{wss} with time and C_w for particle size proportion sets P_{C11} and P_{C12} in particle size combination C_1

	1	D (D 100/)	D (D 150/)
-		$P_{C11} = (P_{4mm \text{ to } 3.15mm} = 10\%) +$	$P_{C12} = (P_{4mm \text{ to } 3.15mm} = 15\%) +$
C_W	Time	$(P_{3.15mm to 0.5mm} = 45\%) +$	$(P_{3.15mm to 0.5mm} = 42.5\%) +$
(%)	(hrs)	$(P_{less than 0.5mm} = 45\%)$	$(P_{less than 0.5mm} = 42.5\%)$
		C _{wss} for P _{C11}	C_{wss} for P_{C12}
	0	49.86%	49.74%
	24	66.99%	64.96%
50	28	66.81%	64.87%
30	48	65.41%	63.95%
	72	64.73%	63.21%
	96	64.73%	63.21%
	0	54.87%	55%
	24	63.26%	63.4%
5.5	28	62.74%	63%
55	48	62.29%	62.61%
	72	62.1%	62.55%
	96	62.1%	62.55%
	0	59.87%	59.75%
	24	64.7%	64.87%
60	28	64.64%	64.76%
00	48	64.56%	64.42%
	72	64.23%	64.25%
	96	64.23%	64.25%
	0	64.88%	64.74%
	24	69.67%	69.39%
65	28	69.57%	69.35%
65	48	68.99%	68.87%
	72	68.49%	68.51%
	96	68.49%	68.51%

From Tables 2 and 3, it can be noted that, for both cases of particle size combinations C_1 and C_2 , static settled concentration increases from 0 hour to 24 hour and then decreases from 24 hour to 72 hour in each case of coking coal concentration (C_w) and particle size proportion sets P_{C11} , P_{C12} , P_{C21} and P_{C22} .

Table 3

Variation of C_{wss} with time and C_w for particle size proportion sets P_{C21} and P_{C22} in particle size combination C_2

		$P_{C21} = (P_{6.7mm \text{ to } 3.15mm} = 10\%) +$	$P_{C22} = (P_{6.7mm \text{ to } 3.15mm} = 15\%) +$
C_{W}	Time	$(P_{3.15mm} \text{ to } 0.5mm = 45\%) +$	$(P_{3.15mm to 0.5mm} = 42.5\%) +$
(%)	(hrs)	$(P_{\text{less than } 0.5\text{mm}} = 45\%)$	$(P_{less than 0.5 mm} = 42.5\%)$
(, 0)	(1115)	C_{wss} for P_{C21}	C_{wss} for P_{C22}
	0	49.79%	49.79%
	24	63.02%	66.22%
	28	62.98%	66.12%
50	48	62.47%	65.61%
	72	62.08%	64.84%
	96	62.08%	64.84%
55	0	54.8%	54.8%
	24	63.19%	63.27%
	24	62.64%	62.87%
	48	63.73%	63.79%
	72	63.33%	63.33%
	96	63.33%	63.33%
	0	59.81%	59.81%
	24	64.81%	65.15%
60	28	64.75%	65.09%
	48	64.7%	64.92%
	72	64.3%	64.36%
	96	64.3%	64.36%
	0	64.82%	64.82%
65	24	68.79%	68.53%
	28	68.63%	68.53%
	48	68.38%	68.23%
	72	67.87%	67.72%
	96	67.87%	67.72%

From Figures 2a and 2b, it can be noted that, for particle size combination C_1 , maximu m static settled concentration (C_{wss}) at 72 hours decreases from $C_w = 50\%$ to 55% and then increases from 55% to 65% for both sets of particle size proportions P_{C11} and P_{C12} . For second particle size combination C_2 , maximum static settled concentration (C_{wss}) at 72 hours increases from $C_w = 50\%$ to 65% for particle size proportions P_{C21} and for P_{C22} , maximum static settled concentration (C_{wss}) at 65% for particle size proportions P_{C21} and for P_{C22} , maximum static settled concentration (C_{wss}) decreases from $C_w = 50\%$ to 55% and then increases from 55% to 65%.

From Figures 2a and 2b, it is observed that, in case of particle size combination C_1 (Figure 2a), with increase in the proportion of coarser particles from particle size proportion set P_{C11} to P_{C12} , the C_{wss} decreases for $C_w = 50\%$ and increases for $C_w = 55\%$, 60% and 65%. While in case of particle size combination C_2 (Figure 2b), with increase in the proportion of coarser particles from particle size proportion set P_{C21} to P_{C22} , C_{wss} increases for $C_w = 50\%$ and 60%, decreases for $C_w = 65\%$ and remain same for $C_w = 55\%$.

From Figure 2a and 2b, it is observed that, in case of particle size combination C_1 (Figure 3a), with increase in the proportion of coarser particles from particle size proportion set P_{C11} to P_{C12} , the C_{wss} decreases for $C_w = 50\%$ and increases for $C_w = 55\%$, 60% and 65%. While in case of particle size combination C_2 (Figure 3b), with increase in the proportion of coarser particles from particle size proportion set P_{C21} to P_{C22} , C_{wss} increases for $C_w = 50\%$ and 60%, decreases for $C_w = 65\%$ and remain same for $C_w = 55\%$.

From Figures 2a and 2b, it is observed that when coarser particle size increases from 4 mm in particle size combination C_1 to 6.7 mm in particle size combination C_2 , the C_{wss} increases for $C_w = 55\%$ and 60% and decreases for $C_w = 50\%$ and 65% in particle size proportion sets P_{C11} and P_{C21} while C_{WSS} increases for $C_w = 50\%$, 55% and 60% and decreases for $C_w = 50\%$, 55% and 60% and decreases for $C_w = 50\%$, 55% and 60% and decreases for $C_w = 65\%$ in particle size proportion sets P_{C12} and P_{C22} .

In both case of particle size combinations C_1 and C_2 and their corresponding particle size proportion sets P_{C11} , P_{C12} , P_{C21} and P_{C22} , the optimum concentration of coking coalwater slurry was found as 55% by weight, as the difference between maximum static settled concentration (C_{wss}) at 72 hours and the slurry concentration (C_w) was within the range of 5% - 10%.



Figure 2. (2a and 2b) Variation of C_{wss} with particle size range proportions P_{C11} and P_{C12} at 72 hours for $C_w = 50\%$, 55%, 60% and 65% by weight in particle size combination C_1

and C₂

4. CONCLUSIONS

From the present study, it is concluded that maximum static settled concentration of coking coal-water slurry at 72 hours increases with increase in coking coal concentration and proportions of particle size ranges in both cases of particle size combinations C_1 and C_2 but this trend is not same for every case of particle size proportion in both particle size combinations C_1 and C_2 . Out of the selected coking coal concentrations, $C_w = 55\%$ is the optimum concentration of coking coal-water slurry in both particle size combinations C_1 and C_2 and their corresponding particle size proportion sets P_{C11} , P_{C12} , P_{C21} and P_{C22} . This study can further be extended for developing a method to optimize the coking coal-water slurries with maximum amount of solid in minimum amount of water and with minimum viscosity for its transportation through pipeline and launder.

REFERENCES

- Biswas, A., Gandhi, B.K., Singh, S.N., Seshadri, V., 2000. Characteristics of coal ash and their role in hydraulic design of ash disposal pipelines. Indian Journal of Engineering & Materials Sciences 7, 1-7.
- 2. Blake, R.O. (Ed.) 1963. Industrial Safety. Prentice Hall, Inc., Englewood Cliffs, N.J.
- 3. Burger, J.H., 2014, Non–Newtonian open channel flow: The effect of shape. Ph.D. thesis, Cape Peninsula University of Technology, Cape Town.
- Faddick, R.R., 1979. The Environmental and Pollution Aspects of Coal Slurry Pipelines. Project report, Industrial Environmental Research Laboratory, Office of Research and Development, U.S. Environmental Protection Agency, Cincinnati, Ohio.
- Gandhi, B.K., Borse, S.V., 2002. Effects of particle size and size distribution on estimating erosion wear of cast iron in sand-water slurries. Indian Journal of Engineering & Materials Sciences 9, 480-486.
- Kaushal, D.R., Seshadri, V., Singh, S.N., 2002. Prediction of concentration and particle size distribution in the flow of multi-sized particulate slurry through rectangular duct. Elsevier, Applied Mathematical Modelling 26, 941-952.
- Leong, Y. K., Creasy, D. E., Boger, D. V., Nguyen, Q. D., 1987. Rheology of brown coal-water suspensions. Rheology Acta 26, 291-300.
- 8. Mishra, R., 1996. Astudy on the flow of multi-sized particulate solid-liquid mixtures in horizontal pipelines. Ph.D. thesis, Indian Institute of Technology, Delhi, India.
- 9. National Academy of Engineering 1974. U.S. Energy Prospects An Engineering Viewpoint. Washington, D.C. p.34.
- Nguyen, Q.D., Logos, C., Semmler, T., 1997. Rheological properties of South Australian coalwater slurries. Coal Preparation 18, 185-199.
- Roh, N. S., Shin, D. H., Kim, D. C., Kim, J. D., 1995. Rheological behavior of coal water mixtures. Effects of coal type, loading and particle size. Fuel 74, 1220-1227.
- Round, G. F., Hessari, A. R., 1987. Rheology of coal slurries, pH and size distribution effects. Particulate and multiphase processes 3, 329-340.
- Sengun, M. Z., Probstein, R. F., 1989. Bimodal model of slurry viscosity with application to coal slurries. Part I, low shear limit behaviour, Rheology Acta 28, 382-401.
- Seshadri, V., Singh, S.N., Ahmed, M., 1997. Prediction of concentration and size distribution of solids in slurry pipeline. Indian Journal of Engineering & Materials Sciences 4, 1-9.
- 15. Singh, H., Kumar, S., Mohapatra, S.K., 2017. Influence of solid concentration on rheological characteristics of fly ash-water suspension. Proc. Int. Conf. on Mechanical, Materials and Renewable Energy. Sikkim, India, 8-10 December 2017.
- Singh, M.K., Ratha, D., Kumar, S., Kumar, D., 2016. Influence of particle-size distribution and temperature on rheological behavior of coal slurry. International Journal of Coal Preparation and Utilization, Taylor and Francis 36, 44-54.
- Toda, M., Kuriyami, M., 1988. The influence of particle size distribution of coal on fluidity of coal water mixtures. Powder Technology 55, 241-247.
- Turian, R. M., Freng-Lung, H., Avramidis, K. S., Allendorfer, R. K., 1992. Settling and rheology of suspensions of narrow sized coal particles. A.I. Ch.E.J 38(7), 969-987.